

A Multigrid LCR-FEM solver for viscoelastic fluids with application to problems with free surface

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Motivation

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Polymer melts:

- One of industrial interests +
- Physically fascinating +
- Rheologically difficult -
- Numerically challenging -





Highly accurate, robust numerical solver which represents the rheological nature is still challenging



Viscoelastic fluid models (D. D. Joseph):

• Integral form

$$\tau(t) = \int_{-\infty}^{t} \frac{1}{We^2} e^{\frac{-(t-s)}{We}} F(s,t) F(s,t)^T \, ds$$

- Differential form: Upper-convected derivative
- More practical to implement than integral form
- Represent many viscoelastic models

$$\frac{\partial \tau}{\partial t} + (u \cdot \nabla)\tau - \nabla u \cdot \tau - \tau \cdot \nabla u^T = f(\tau)$$

- Conformation tensor (τ), velocity (u), source ($f(\tau)$)
- Not able to capture high stress gradient at higher We number
- $f(\tau)$ can be Oldroyd-B, Giesekus, FENE, PTT, WM, Pom-Pom

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Numerical Results



Cells stress11 -2.57e+03 -2.31e+03 Cutline of Stress_11 -2.05e+03 component at y = 1.0We = 1.5 with -1.8e+03 -1.54e+03 LCR -1.28e+03 -1.03e+03**Old Formulation Vs Lcr** - 770 - 513 → We= 0.5 → We= 1.5 257 Cells stress11 124 2995 - 111 2495 - 98.6 1995 S 1495 - 86.1 stres We = 0.5 with 995 - 73.7 495 **Old formulation** - 61.2 - 48.7 0.20 0,40 0,60 0,80 1.00 0,00 X - 36.2 - 23.7 - 11.2

--1.26



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Experience (Kupferman et. al):

- Stresses grow exponentially
- Conformation tensor looses positive properties during numerics

$$\begin{aligned} \frac{\partial \tau}{\partial t} + (u \cdot \nabla)\tau - \nabla u \cdot \tau - \tau \cdot \nabla u^T &= f(\tau) \\ \nabla u &= \Omega + B + N\tau^{-1} \\ \frac{\partial \tau}{\partial t} + (u \cdot \nabla)\tau - (\Omega\tau - \tau\Omega) - 2B\tau &= f(\tau) \\ \tau &= e^{\psi} \\ \frac{\partial \psi}{\partial t} + (u \cdot \nabla)\psi - (\Omega\psi - \psi\Omega) - 2B &= g(\psi) \end{aligned}$$



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LCR based viscoelastic fluid:

- Ability to capture high stress gradients at higher We number
- Positivity preserving by design $\tau = e^{\psi}$
- Numerically more stable with appropriate FEM

$$\frac{\partial \psi}{\partial t} + (u \cdot \nabla)\psi - (\Omega \psi - \psi \Omega) - 2B = g(\psi)$$

- LCR tensor (ψ), velocity (u), source ($g(\psi)$)
- $\nabla u = \Omega + B + N\tau^{-1}$
- $g(\psi)$ can be Oldroyd-B, Giesekus, FENE, PTT, WM, Pom-Pom \mathfrak{S}^*



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LCR based viscoelastic fluid:

Model	$f(\mathbf{\tau})$	g(ψ)
OdB	$1/\lambda (\mathbf{I} - \boldsymbol{\tau})$	$1/\lambda (\exp(-\psi) - \mathbf{I})$
Gie	$1/\lambda \left(\mathbf{I}-\boldsymbol{\tau}-\boldsymbol{\alpha}(\boldsymbol{\tau}-\mathbf{I})^2\right)$	$1/\lambda (\exp(-\psi) - \mathbf{I}) - \alpha \exp(\psi)(\exp(-\psi) - \mathbf{I})^2)$
FENE	$-1/\lambda (f(\mathbf{R})\boldsymbol{\tau} - \alpha f(\mathbf{R})\mathbf{I})$	$-1/\lambda (f(\mathbf{R}) - \alpha f(\mathbf{R}) \exp(-\psi))$
LPTT	$-1/\lambda (1+\epsilon(\operatorname{tr}(\boldsymbol{\tau})-3))(\mathbf{I}-\boldsymbol{\tau})$	$-1/\lambda (1 + \varepsilon(tr(exp(\psi)) - 3))(exp(-\psi) - \mathbf{I})$
XPTT	$-1/\lambda (\exp(\varepsilon(tr(\tau)-3)))(\mathbf{I}-\tau)$	$-1/\lambda (\exp(\epsilon(tr(\exp(\psi)) - 3)))(\exp(-\psi) - \mathbf{I})$
WM	$-1/\lambda(\dot{\gamma}) (\boldsymbol{\tau} - \mathbf{I})$	$-1/\lambda(\dot{\gamma}) \left(\mathbf{I} - \exp(-\mathbf{\psi})\right)$
Pom	$-1/\lambda_{\mathbf{b}}(\mathbf{f}(\boldsymbol{\tau})-2\alpha+\alpha\boldsymbol{\tau}+(\alpha-1)\mathbf{I})$	$-1/\lambda_{\mathbf{b}}(\mathbf{f}(\mathbf{\psi}) - 2\alpha + \alpha \exp(\mathbf{\psi}) + (\alpha - 1)\exp(-\mathbf{\psi}))$

• Relaxation time (λ)



Multiphysics flow model



- Navier-Stokes equation (u, p) $\rho\left(\frac{\partial}{\partial t} + u \cdot \nabla\right) u = -\nabla p + \nabla \cdot \sigma_s + \frac{1}{\lambda} \nabla \cdot \eta_p e^{\psi}, \qquad \nabla \cdot u = 0$
 - + Nonlinear viscosities

$$\sigma_s = 2\eta_s(\dot{\gamma}, \Theta, p)D, \ \dot{\gamma} = \sqrt{tr(D^2)}$$

+ Temperature effects with Boussinesq and viscous dissipation (Θ)

$$\rho c_p \left(\frac{\partial}{\partial t} + u \cdot \nabla \right) \Theta = k_1 \nabla^2 \Theta + k_2 D : D$$

• + Viscoelastic fluid models (ψ)

$$\frac{\partial \psi}{\partial t} + (u \cdot \nabla)\psi - (\Omega \psi - \psi \Omega) - 2B = g(\psi)$$

+ Multiphase flow with Level-Set equation

$$\frac{\partial \varphi}{\partial t} + (u \cdot \nabla)\varphi = 0$$



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In Time:

- Second order Crank-Nicolson
- Can be adaptively applied

In Space: Higher order finite element (Arnoldi)

- Inf-sup stable for velocity and pressure
- High order: good for accuracy
- Discontinuous pressure: good for solver & physics
- Edge oriented FEM for numerical stabilitation (Burman)





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Saddle point problem:

- \tilde{u} consists of all numerical variables except pressure
- Newton with multigrid as well-known solver
- Monolithic way of solving

$$\begin{pmatrix} A & B^T \\ B & 0 \end{pmatrix} \begin{pmatrix} \widetilde{u} \\ p \end{pmatrix} = \begin{pmatrix} \operatorname{rhs}_{\widetilde{u}} \\ \operatorname{rhs}_p \end{pmatrix}$$

- A consists of differential operators
- *B* is gradient operator



Newton iteration

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Newton for nonlinear system:

- Strongly coupled problem
- Automatic damping control ω^n for each nonlinear step
- Black-box for many given viscoelastic models

$$x^{n+1} = x^n + \omega^n \left[\frac{\partial \mathcal{R}(x^n)}{\partial x}\right]^{-1} \mathcal{R}(x^n)$$

- Quadratic convergence when iterative solutions are close
- Solution $x^{n+1} = (\tilde{u}, p)$, Residual equation $\mathcal{R}(x^n)$
- Black-box is made possible by divided difference technique

$$\left[\frac{\partial \mathcal{R}(x^n)}{\partial x}\right]_{ij} = \frac{\mathcal{R}_i(x^n + \varepsilon e_j) - \mathcal{R}_i(x^n + \varepsilon e_j)}{2\varepsilon}$$

Multigrid iteration

Multigrid for linearized system:

- Full-Vanka for strongly coupled Jacobian in local system
- Full prolongation
- Black-box for many given viscoelastic models









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Flow around cylinder:



Mod.	Gie	FENE-P	FENE-C	WM-Lr	WM-Cr	WM-Ca	LPPT/ XPPT	Pom
Par	α=0.01	α = 0, L2=100	α = 1, L2=100	I=0.01	k=0.01, l=0.01, m=0.01, n=0.01	a = 0.95, b = 0.95, k= 0.01, l = 0.01, m = 0.01, n = 0.01	ε=0.01	α=0.01, v = 0.2, r = 1



Flow around cylinder:

Lev.	Oldroyd-B	Giesekus	FENE-P	FENE-CR	LPTT
R1	126.5259[5/1]	126.0070[5/1]	125.3255[5/1]	126.6369[5/1]	126.5436[5/1]
R2	128.9641[5/1]	128.3420[4/1]	127.6645[5/1]	129.0771[5/1]	128.9727[5/1]
R3	129.9711[3/1]	129.2975[3/1]	128.6161[3/1]	130.0719[3/1]	129.9712[3/1]
R4	130.2648[2/2]	129.5757[2/2]	128.8925[2/2]	130.3606[2/2]	130.2608[2/2]
R5	130.3388[2/2]	129.6466[2/2]	128.9632[2/2]	130.4338[2/2]	130.3341[2/2]
	XPTT	WM-Larson	WM-Cross	WM-Carreau	Pom-Pom
R1	126.5437[5/1]	126.3346[5/1]	124.6317[5/1]	124.3082[5/1]	126.0887[4/1]
R2	128.9728[5/1]	128.7564[4/1]	126.9133[5/1]	126.5703[5/1]	128.3629[5/1]
R3	129.9713[3/1]	129.7564[3/1]	127.8540[3/1]	127.5025[3/1]	129.1754[3/1]
R4	130.2608[2/2]	130.0482[2/2]	128.1303[2/2]	127.7764[2/2]	129.4095[2/2]
R5	130 3342[2/2]	130 1219[2/2]	128 2007[2/2]	127 8463[2/2]	129 4728[2/2]

Newton-multigrid behaviour for We=0.1



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Flow around cylinder:

We	Oldroyd-B	Giesekus	FENE-P	FENE-CR	LPTT
0.6	117.7887[2]	111.9109[2]	114.0870[2]	119.6564[2]	119.2840[2]
0.7	117.3345[3]	110.4256[3]	113.1044[3]	119.4340[3]	119.0223[3]
0.8	117.3718[3]	109.2601[3]	112.4831[3]	119.5552[3]	119.1038[3]
0.9	117.8039[4]	108.3084[3]	112.1125[4]	119.9018[4]	119.4197[3]
1.0	118.5410[3]	107.5035[3]	111.9158[4]	120.3899[4]	119.8937[3]
1.1	119.5344[3]	106.8035[3]	111.8408[4]	120.9640[4]	120.4741[3]
1.2	120.7520[5]	106.1817[5]	111.8526[3]	121.5885[3]	121.1270[3]
	VDTT				
	APTI	www-larson	WW-Cross	www-Carreau	Pom-Pom
0.6	APT1 119.4010[2]	117.1221[2]	116.6605[2]	116.4609[2]	104.9392[4]
0.6 0.7	119.4010[2] 119.1871[3]	117.1221[2] 116.5785[3]	116.6605[2] 116.2328[3]	116.4609[2] 116.0340[3]	104.9392[4] 102.8783[3]
0.6 0.7 0.8	XP11 119.4010[2] 119.1871[3] 119.3129[3]	117.1221[2] 116.5785[3] 116.5114[3]	116.6605[2] 116.2328[3] 116.2700[3]	116.4609[2] 116.0340[3] 116.0675[3]	Pom-Pom 104.9392[4] 102.8783[3] 101.2295[3]
0.6 0.7 0.8 0.9	XP11 119.4010[2] 119.1871[3] 119.3129[3] 119.6645[3]	117.1221[2] 116.5785[3] 116.5114[3] 116.8218[4]	116.6605[2] 116.2328[3] 116.2700[3] 116.6810[4]	116.4609[2] 116.0340[3] 116.0675[3] 116.4717[4]	Pom-Pom 104.9392[4] 102.8783[3] 101.2295[3] 99.8823[3]
0.6 0.7 0.8 0.9 1.0	XP11 119.4010[2] 119.1871[3] 119.3129[3] 119.6645[3] 120.1624[3]	117.1221[2] 116.5785[3] 116.5114[3] 116.8218[4] 117.4164[3]	116.6605[2] 116.2328[3] 116.2700[3] 116.6810[4] 117.3786[3]	116.4609[2] 116.0340[3] 116.0675[3] 116.4717[4] 117.1597[3]	Pom-Pom 104.9392[4] 102.8783[3] 101.2295[3] 99.8823[3] 98.7611[3]
0.6 0.7 0.8 0.9 1.0 1.1	XP11 119.4010[2] 119.1871[3] 119.3129[3] 119.6645[3] 120.1624[3] 120.7540[3]	117.1221[2] 116.5785[3] 116.5114[3] 116.8218[4] 117.4164[3] 118.2415[3]	116.6605[2] 116.2328[3] 116.2700[3] 116.6810[4] 117.3786[3] 118.3140[3]	116.4609[2] 116.0340[3] 116.0675[3] 116.4717[4] 117.1597[3] 118.0826[3]	Pom-Pom 104.9392[4] 102.8783[3] 101.2295[3] 99.8823[3] 98.7611[3] 97.8127[3]

Moderate number of nonlinear steps for all models



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Flow around cylinder:



Different drag behaviour of different models at increasing We number



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Rising bubble in viscoelastic fluid:



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Rising bubble in viscoelastic fluid:



- A better visualisation from the data before. ",cheating bubbles"
- Multiphase flow in a cylindrical coordinate system is ongoing



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3D flow around a sphere:

- An LCR based FEM solver for 3D viscoelastic flow
- Tests with Oldroyd-B for We=0.3 and 0.6



We=0.3

We=0.6

Resolution	$\max_1(\tau_{xx})$	$\max_2(\tau_{xx})$	F^*
L2	20.80	2.082	5.6976
L3	19.29	2.081	5.6946
L4	18.72	2.086	5.6941
L5	18.52	2.087	5.6940
Authors		Reference values	
Lunsmann [4]	-	-	5.6937
Owens [5]	18.27	-	5.6963

Resolution	$\max_1(\tau_{xx})$	$\max_2(\tau_{xx})$	F^*
L2	50.31	5.041	5.4170
L3	39.01	5.061	5.4133
L4	36.43	5.104	5.4128
L5	35.65	5.118	5.4128
Authors		Reference values	
Lunsmann [4]	35.17	-	5.4123
Owens [5]	35.67	-	5.4117
Sahin [6]	34.73	5.12	-

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3D flow around cylinder:

- An LCR based FEM solver for 3D viscoelastic flow
- Tests with Oldroyd-B
- Invariance in z-direction for We=1.6, agreement with Sahin et. al





Polymer stretching:

• A 2D+1 membrane model (Sollogoub et. Al)

$$\nabla \cdot eU = 0$$

$$\nabla \cdot e(2\mu D + 2\mu tr(D)I) = \nabla \cdot e\tau$$

$$\frac{\partial \tau}{\partial t} + (U \cdot \nabla)\tau - \nabla U \cdot \tau - \tau \cdot \nabla U^{T} = \frac{1}{\lambda}f$$

• Level set-FEM

$$\frac{\partial \varphi}{\partial t} + (U \cdot \nabla)\varphi = 0$$





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Polymer stretching:

• A 2D+1 membrane model from Sollogoub et. al



Conclusion

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We have presented:

- LCR-based viscoelastic models
- Higher order FEM discretizations
- Black-box Newton-multigrid solver
- Numerical examples:
 - o 2D benchmark flow around cylinder
 - Rising bubble surrounded by viscoelastic fluid
 - 3D solver for LCR-based viscoelastic models
 - Polymer stretching

We would like in the future:

- 3D viscoelatic multiphase
- Collection of different viscoelastic models
- FBM and viscoelastic integral model







