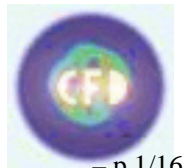


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# ***Efficient Numerical Methods and Simulation techniques for Granular flow***

Abderrahim Ouazzi, Stefan Turek

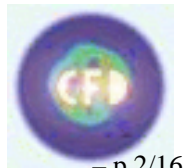
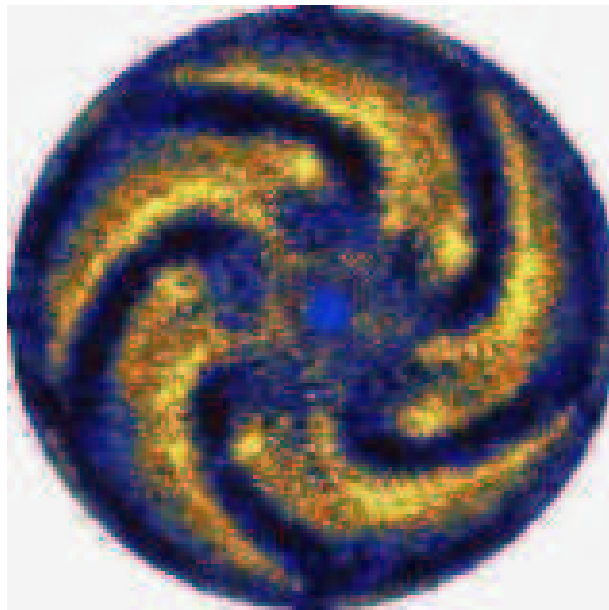
Institut für Angewandte Mathematik und Numerik, LS3,  
Universität Dortmund,  
Germany



# *Examples of Applications*

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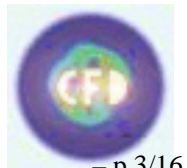
- **Paddles in a mixer or granulator**



# *Examples of Applications*

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- **Flow around inserts during emptying of bins and hoppers**



# Schaeffer Law

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- Incompressible Stokes problem

$$-\nabla \cdot [2\nu(D_{\parallel}(u), p)\mathbf{D}(u)] + \nabla p = f, \quad \nabla \cdot \mathbf{u} = 0 \quad (1)$$

the nonlinear viscosity  $\nu(\cdot, \cdot)$  is a function of  $D_{\parallel}(u)$  and  $p$ ,

$$D_{\parallel}(u) = \frac{1}{2}D(u) : D(u) = \frac{1}{2} \sum_{i,j} D_{i,j}(u)D_{i,j}(u).$$

- Power law defined for

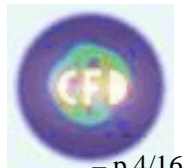
$$\nu(z, p) = \nu_0 z^{\frac{r}{2}-1}$$

- Bingham law defined for

$$\nu(z, p) = \nu_0 z^{\frac{-1}{2}}$$

- Schaeffer law (including the pressure) defined for

$$\nu(z, p) = pz^{\frac{-1}{2}}$$



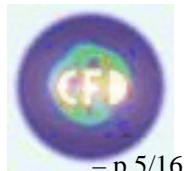
# Nonlinear Solver

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Let  $\mathbf{u}^l$  being the initial state, the (continuous) Newton method consists of finding  $\mathbf{u}$  such that

$$\begin{aligned} & \int_{\Omega} 2\nu(D_{\mathbf{I}}(\mathbf{u}^l), p^l) \mathbf{D}(\mathbf{u}) : \mathbf{D}(\mathbf{v}) dx \\ & + \int_{\Omega} 2\partial_1 \nu(D_{\mathbf{I}}(\mathbf{u}^l), p^l) [\mathbf{D}(\mathbf{u}^l) : \mathbf{D}(\mathbf{u})] [\mathbf{D}(\mathbf{u}^l) : \mathbf{D}(\mathbf{v})] dx \\ & + \int_{\Omega} 2\partial_2 \nu(D_{\mathbf{I}}(\mathbf{u}^l), p^l) [\mathbf{D}(\mathbf{u}^l) : \mathbf{D}(\mathbf{v})] p dx \\ & = \int_{\Omega} \mathbf{f} \mathbf{v} - \int_{\Omega} 2\nu(D_{\mathbf{I}}(\mathbf{u}^l), p^l) \mathbf{D}(\mathbf{u}^l) : \mathbf{D}(\mathbf{v}) dx, \quad \forall \mathbf{v} \in V, \quad (2) \end{aligned}$$

where  $\partial_i \nu(\cdot, \cdot); i = 1, 2$  is the partial derivative of  $\nu$  related to the first and second variable respectively.



# New Linear Algebraic Problem

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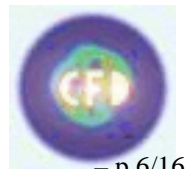
The algorithm consists of finding  $(\mathbf{u}, p)$  as solution of the linear system

$$\begin{cases} A(\mathbf{u}^l, p^l)\mathbf{u} + \delta_d A^*(\mathbf{u}^l, p^l)\mathbf{u} + Bp + \delta_p B^*(\mathbf{u}^l, p^l)p & = R_u(\mathbf{u}^l, p^l), \\ B^T \mathbf{u} & = R_p(\mathbf{u}^l, p^l), \end{cases} \quad (3)$$

where  $R_u(\cdot, \cdot)$  and  $R_p(\cdot, \cdot)$  denote the corresponding nonlinear residual terms for the momentum and continuity equations, and the matrix  $A^*(\mathbf{u}^l, p^l)$  and  $B^*(\mathbf{u}^l, p^l)$  are defined as follows respectively

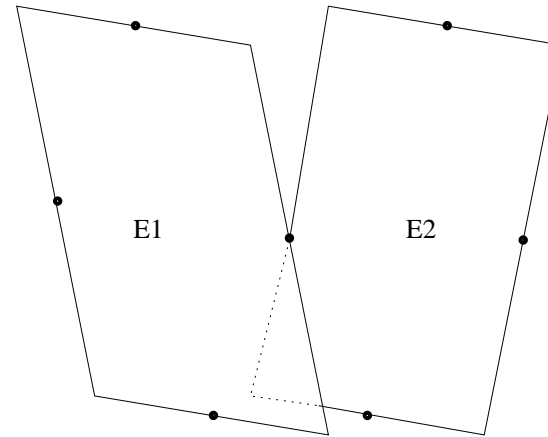
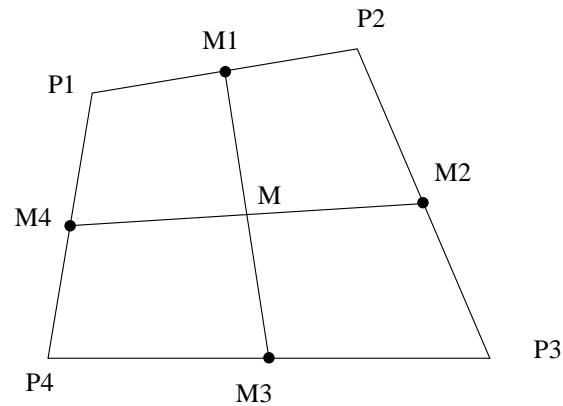
$$\langle A^*(\mathbf{u}^l, p^l)\mathbf{u}, \mathbf{v} \rangle = \int_{\Omega} 2\partial_1 \nu(D_{\mathbf{I}}(\mathbf{u}^l), p^l)[D(\mathbf{u}^l) : D(\mathbf{u})][D(\mathbf{u}^l) : D(\mathbf{v})] dx. \quad (4)$$

$$\langle B^*(\mathbf{u}^l, p^l)p, \mathbf{v} \rangle = \int_{\Omega} 2\partial_2 \nu(D_{\mathbf{I}}(\mathbf{u}^l), p^l)[D(\mathbf{u}^l) : D(\mathbf{v})] p dx. \quad (5)$$



# Spatial discretization

## Quadrilateral Rannacher-Turek Stokes Element



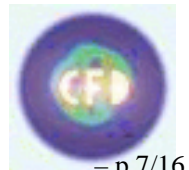
## Advantage:

- Stable and efficient for incompressible flow.
- Compact data structures.

## Disadvantage: "Not" satisfying discrete Korn's inequality

$$\sum_{\tau \in \mathcal{T}_h} \|v\|_{H^1(\tau)} \leq c(\|v\|_{0,\tau}^2 + \|D(v)\|_{0,\tau}^2)^{\frac{1}{2}}$$

(6)



# Stabilized Rannacher-Turek Stokes Element

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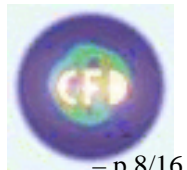
## ● Remedy: Stabilized R-T FEM

The stabilization consists of adding the following bilinear form

$$\sum_{E \in E_I \cup E_D} \frac{1}{|E|} \int_E [\phi_i][\phi_j] ds \quad (7)$$

for all basis function  $\phi_i$  and  $\phi_j$  with a weighted parameter  $s = s(\nu)$  which will act as 'free' stabilization parameter. Then the corresponding matrix  $S$  is defined as:

$$\langle Su, v \rangle = \sum_{E \in E_I \cup E_D} \frac{1}{|E|} \int_E [u][v] ds \quad (8)$$



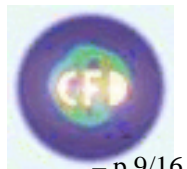


# Linear Multigrid solver

- Vanka smoother as defect correction

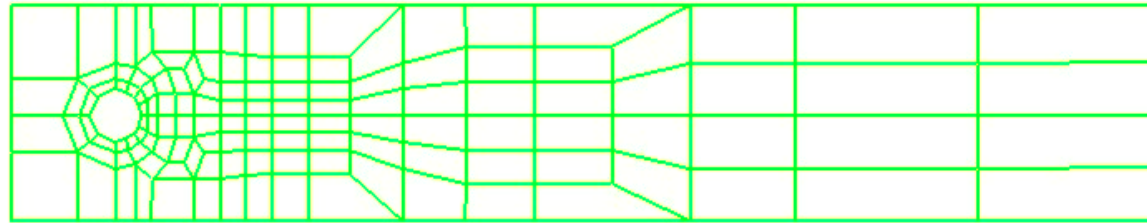
$$\begin{bmatrix} \mathbf{u}^{l+1} \\ p^{l+1} \end{bmatrix} = \begin{bmatrix} \mathbf{u}^l \\ p^l \end{bmatrix} + \omega^l \sum_i \begin{pmatrix} F + S^*_{|\Omega_i} & \tilde{B} + \delta_p \tilde{B}^*_{|\Omega_i} \\ \tilde{B}^T_{|\Omega_i} & 0 \end{pmatrix}^{-1} \begin{bmatrix} \tilde{R}_u(\mathbf{u}^l, p^l) \\ \tilde{R}_p(\mathbf{u}^l, p^l) \end{bmatrix} \quad (9)$$

with matrix  $F = \tilde{A} + \delta_d \tilde{A}^*$ . For the preconditioning step only a part of the matrix, i.e.  $F + S^*$ , is taken

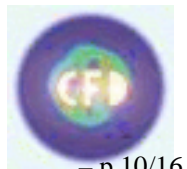


# Comparison with high order scheme

- Coarse mesh and geometrical details for 'Flow around a cylinder'

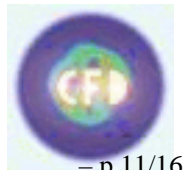


Mesh information			$\tilde{Q}_1/Q_0$	$Q_2/P_1$
Level	Elements	Vertices	Total unknowns	Total unknowns
1	156	130	702	1533
2	572	520	2686	5927
3	2184	2080	10608	23295
4	8528	8320	42016	92351
5	33696	33280	167232	367743
6	133952	133120	667264	—



# Comparison with high order scheme

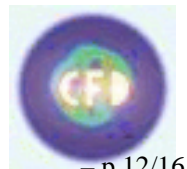
$\nu(D_{\parallel}, p) = (\epsilon + D_{\parallel}(u))^{-\alpha/2}$					
Level	Elements	Drag	Lift	$\Delta p$	NNL/AVL
$\alpha = 0.9$					
2	$\tilde{Q}_1/Q_0$	819.49	2.5201	14.22	13/2
	$Q_2/P_1$	920.59	2.1805	16.76	14/27
3	$\tilde{Q}_1/Q_0$	917.89	3.1958	15.54	14/2
	$Q_2/P_1$	941.51	3.3310	16.02	15/70
4	$\tilde{Q}_1/Q_0$	916.02	3.7381	15.74	12/2
	$Q_2/P_1$	953.94	3.9217	15.82	16/208
5	$\tilde{Q}_1/Q_0$	935.13	3.9954	15.82	15/3
	$Q_2/P_1$	957.64	4.0587	15.87	33/368
6	$\tilde{Q}_1/Q_0$	946.22	4.0592	15.85	13/5



# Efficiency of the nonlinear solver

## Shear dependent viscosity flow

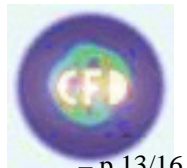
$\nu(D_{\parallel}, p) = (\epsilon + D_{\parallel}(u))^{-\alpha/2}$				
$\tilde{Q}_1/Q_0$				
$\alpha$	0.9			
$\epsilon = 10^{-2}$	Newton		Fixpoint	
Level	NNL/AVL	CPU	NNL/AVL	CPU
2	13/2	60	74/2	228
3	14/2	215	114/2	1359
4	12/2	740	125/2	5871
5	15/3	3957	119/2	21735
6	13/5	25926	109/2	80438



# Efficiency of the nonlinear solver

- Shear dependent viscosity flow

$\nu(D_{\parallel}, p) = (\epsilon + D_{\parallel}(u))^{-\alpha/2}$				
$\epsilon = 10^{-2}$	Newton		Fixpoint	
$\alpha$	NNL/AVL	CPU	NNL/AVL	CPU
0.1	7/2	7	10/2	9
0.5	7/2	8	27/2	32
0.9	9/3	16	113/3	190
1.0	12/4	52	394/2	889



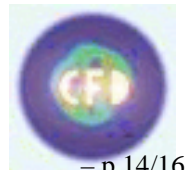
# Efficiency of the nonlinear solver

## ● Pressure dependent viscosity flow

$\nu(D_{\mathbf{I}}, p) = \exp(\beta p)$	Newton		Fixpoint	
$\beta$	NNL/AVL	CPU	NNL/AVL	CPU
$5 \times 10^{-2}$	5/2	9	10/2	21
$1 \times 10^{-1}$	6/2	13	15/2	33
$2 \times 10^{-1}$	7/4	33	30/3	86

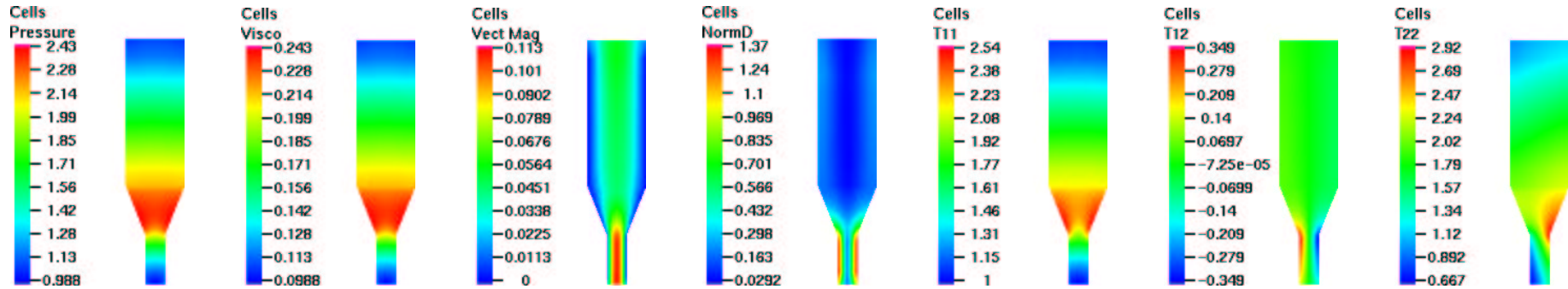
$\nu(D_{\mathbf{I}}, p) = \beta p$	Newton		Fixpoint	
$\beta$	NNL/AVL	CPU	NNL/AVL	CPU
$5 \times 10^{-2}$	9/6	63	94/4	296
$1 \times 10^{-1}$	8/7	65	103/4	426
$2 \times 10^{-1}$	7/16	120	124/8	1042



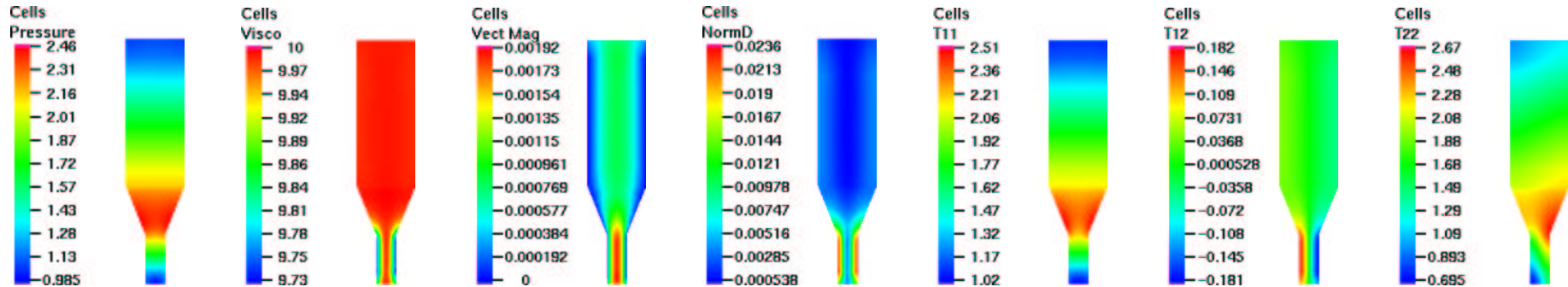
# Steady state flow in Silos

Schaeffer flow under gravity force

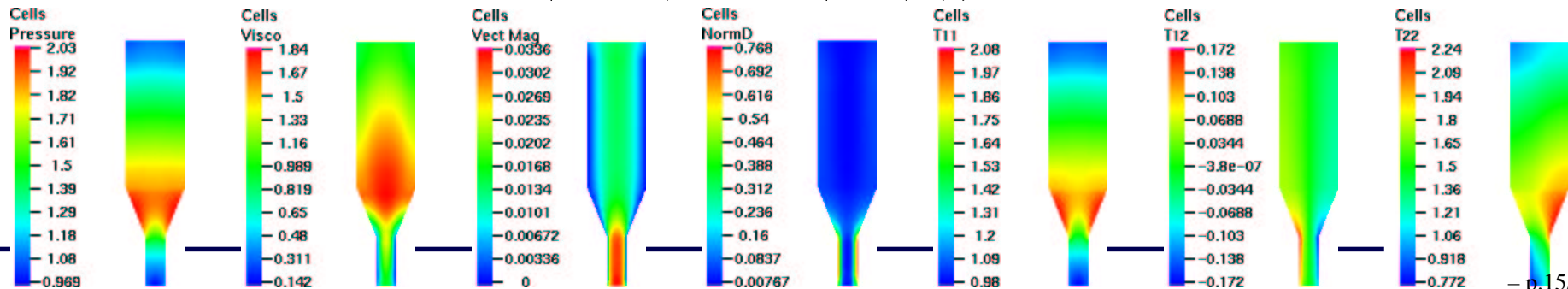
$$\nu(D_{\mathbb{I}}, p) = \beta p$$



$$\nu(D_{\mathbb{I}}, p) = (D_{\mathbb{I}}(u))^{-1/2}$$

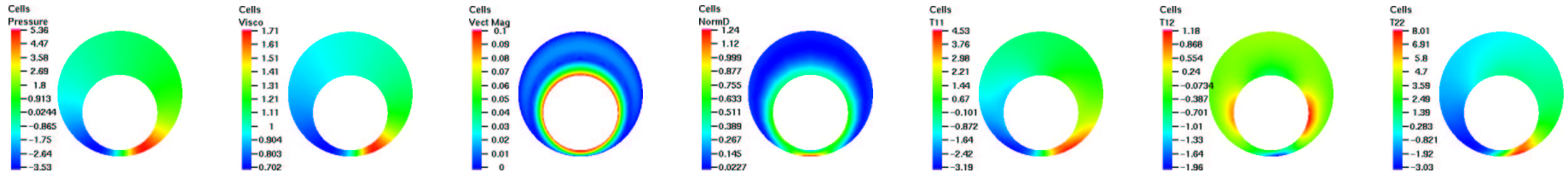


$$\nu(D_{\mathbb{I}}, p) = \beta p (D_{\mathbb{I}}(u))^{-1/2}$$

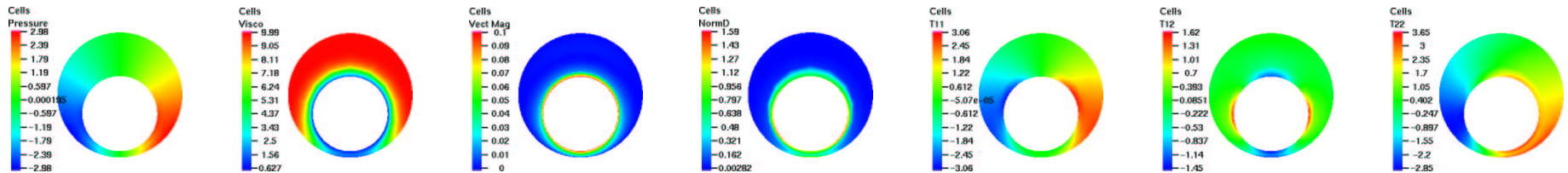


# Steady state flow in Couette device

$$\nu(D_{\parallel}, p) = \exp(\beta p)$$



$$\nu(D_{\parallel}, p) = (D_{\parallel}(u))^{-1/2}$$



$$\nu(D_{\parallel}, p) = \exp(\beta p)(D_{\parallel}(u))^{-1/2}$$

