FEM Techniques for Particulate Flow

Stefan Turek, Decheng Wan

Institut für Angewandte Mathematik, Univ. Dortmund http://www.mathematik.uni-dortmund.de/LS3 http://www.featflow.de



Model for particulate flow

Numerical techniques



Fluid – (Rigid) Solid Interfaces

Consider flow of N solid particles in a fluid with density ρ and viscosity μ . Denote by $\Omega_f(t)$ the domain occupied by the fluid at time t, and by $\Omega_p(t)$ domain occupied by the particle p at time t:



Fluid flow is modelled by the **Navier-Stokes equations** in $\Omega_f(t)$

$$\rho \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) - \nabla \cdot \sigma = \mathbf{f}, \qquad \nabla \cdot \mathbf{u} = 0$$

where σ is the total stress tensor in the fluid phase, which is defined as :

$$\sigma(X, t) = -p \mathbf{I} + \mu \left[\nabla \mathbf{u} + (\nabla \mathbf{u})^T \right]$$

Model for Particle Motion (I)

Motion of particles is described by the Newton-Euler equations, i.e., the translational velocities U_p and angular velocities ω_p of the *p*-th particle satisfy

$$M_p \frac{d U_p}{d t} = F_p + F'_p + (\Delta M_p) \mathbf{g}, \qquad \mathbf{I}_p \frac{d \omega_p}{d t} + \omega_p \times (\mathbf{I}_p \omega_p) = T_p$$

with M_p the mass of the *p*-th particle (*p*=1,...,N); I_p the moment of inertia tensor of the *p*-th particle;

 ΔM_p the mass difference between the mass M_p and the mass of the fluid occupying the same volume.

 F_p and T_p are the **hydrodynamical forces** and the **torque** at mass center acting on the *p*-th particle

$$F_p = -\int_{\Gamma_p} \sigma \cdot \mathbf{n}_p \, d\,\Gamma_p \,, \qquad T_p = -\int_{\Gamma_p} (X - X_p) \times (\sigma \cdot \mathbf{n}_p) \, d\,\Gamma_p$$

and F'_p are the collision forces (later).

 X_p is the position of the center of gravity of the *p*-th particle; $\Gamma_p = \partial \Omega_p$ the boundary of the *p*-th particle; \mathbf{n}_p is the unit normal vector on the boundary Γ_p

Interaction between Particle and Fluid

No slip boundary conditions at interface Γ_p between particles and fluid i.e., for any $X \in \Gamma_p$, the velocity $\mathbf{u}(X)$ is defined by:

$$\mathbf{u}(X) = U_p + \omega_p \times (X - X_p)$$

The **position** X_p of the *p*-th particle and its **angle** θ_p are obtained by integration of the kinematic equations:

$$\frac{d X_p}{d t} = U_p , \qquad \frac{d \theta_p}{d t} = \omega_p$$

Coupling between Fluid and Particle

1. **Implicit coupling** (``Distributed Lagrange Multiplier/Fictitious Domains``)

Idea: Calculate the fluid on the complete fluid-solid domain; the solid domain is constrained to move with the rigid motion; mutual forces between solid and fluid are cancelled.

- Body-force-DLM (Glowinski,Pan,Hesla,Joseph and Periaux (1999)): the constraint of rigid body motion is represented by $u=U+\omega \times r$
- Stress-DLM (Patankar,Singh,Joseph,Glowinski and Pan (2000)): the constraint of the rigid body motion is represented by a stress field just as there is pressure in fluid.

2. Explicit coupling

$$t^n$$
 fluid \rightarrow t^n force on solid \rightarrow t^{n+1} solid \rightarrow t^{n+1} fluid



FVM-fictitious domain methods (Duchanoy and Jongen(2003))

FEM-fictitious boundary methods (Turek, Wan and Rivkind)

The 'Fictitious Boundary Method (FBM)'

1. Describe fine-scale geometrical structures and time-dependent objects via (level-dependent) inner "boundary points"!

2. Use projectors onto the "right" b.c.'s in iterative components!



Computational mesh (can be) independent of 'internal objects'

How to Calculate Forces with FBM?

Hydrodynamic forces and torque acting on the i-th particle

$$\mathbf{F}_{i} = -\int_{\partial P_{i}} \boldsymbol{\sigma} \cdot \mathbf{n}_{i} \, d \, \Gamma_{i} \,, \qquad T_{i} = -\int_{\partial P_{i}} (\mathbf{X} - \mathbf{X}_{i}) \times (\boldsymbol{\sigma} \cdot \mathbf{n}_{i}) \, d \, \Gamma_{i}$$



FBM: Reconstruction of the shape is only first order accurate
→ local grid adaptivity or alignment
→ "only" averaged/integral quantities are required



But: The FBM can only decide "INSIDE" or "OUTSIDE"

'Replace the surface integral by a volume integral'

Calculation of Hydrodynamic Forces

Define auxiliary function α as

$$\alpha_p(X) = \begin{cases} 1 & \text{for} \quad X \in \Omega_p \\ 0 & \text{for} \quad X \in \Omega_f \end{cases}$$

Remark: $\nabla \alpha_p = 0$ everywhere except at wall surface of the particles, and equal to the normal vector \mathbf{n}_p defined on the global grid.

$$\mathbf{n}_p = \nabla \alpha_p$$

Force acting on the wall surface of the particles can be computed by

$$F_p = -\int_{\Gamma_p} \sigma \cdot \mathbf{n}_p \, d\,\Gamma_p = -\int_{\Omega_T} \sigma \cdot \nabla \alpha_p \, d\,\Omega_T$$

with $\bar{\Omega}_T = \bar{\Omega}_f \cup \bar{\Omega}_p$ (analogously for the torque)

Evaluation of Force Calculations

LEVEL $6 \approx 280.000$ elements

LEVEL 6 \approx 150.000 elements

LEVEL	ch. mesh I	ch. mesh II	ch. mesh I	ch. mesh II		
3	0.5529+01	0.5569+01	0.1216-01	0.2443-03		
4	0.5353+01	0.5575+01	0.1074-01	0.0014-01		
5	0.5427+01	0.5572+01	0.6145-02	0.0812-01		
6	0.5501+01	0.5578+01	0.9902-02	0.1020-01		
	$C_d = 0.5$	55795+01	$C_l = 0.10618-01$			



LEVEL	C_d	C_l
2	0.55201+01	0.1057-01
3	0.55759+01	0.1036-01
4	0.55805+01	0.1041-01

LEVEL $4 \approx 150.000$ elements

(Explicit) Operator-Splitting Approach

The algorithm for $t^n \rightarrow t^{n+1}$ consists of the following 4 substeps

- 1. Fluid velocity and pressure : $NSE(\mathbf{u}_{f}^{n+1}, p^{n+1}) = BC(\Omega_{p}^{n}, \mathbf{u}_{p}^{n})$
- 2. Calculate hydrodynamic forces: $\mathbf{F_p}^{n+1}$
- 3. Calculate velocity of particles: $\mathbf{u}_p^{n+1} = g(\mathbf{F}_{\mathbf{p}}^{n+1})$
- 4. Update position of particles: $\Omega_p^{n+1} = f(\mathbf{u}_p^{n+1})$

→ Required: efficient calculation of hydrodynamic forces
→ Required: efficient treatment of particle interaction (?)
→ Required: fast (nonstationary) Navier-Stokes solvers (!)

'One particle in a rotating circular container'



 $R_{\Omega} = 2.0, \quad R_p = 1.0$



'One ellipse falling in an (infinite) channel'







Lift-Off for Circle



Lift-Off for Ellipse



Velocity $(d_w = 0.4)$

Velocity $(d_w = 1.8)$



'Kissing, Drafting, Thumbling'



'Impact of heavy balls on 2000 small particles'



Collision Models

- Theoretically, it is impossible that smooth particle-particle collisions take place in finite time in the continuous system since there are repulsive forces to prevent these collisions in the case of viscous fluids.
 - In practice, however, particles can contact or even overlap each other in **numerical simulations** since the gap can become arbitrarily small due to unavoidable numerical errors.



Repulsive Force Collision Model

Handling of small gaps and contact between particles

Dealing with overlapping in numerical simulations

For the particle-particle collisions (analogous for the particle-wall collisions), the repulsive forces between particles read:

$$\mathbf{F}_{i,j}^{P} = \begin{cases} 0 & \text{for } d_{i,j} > R_i + R_j + \rho \\ \frac{1}{\epsilon_P} (\mathbf{X}_i - \mathbf{X}_j) (R_i + R_j + \rho - d_{i,j})^2 & \text{for } R_i + R_j \le d_{i,j} \le R_i + R_j + \rho \\ \frac{1}{\epsilon_P'} (\mathbf{X}_i - \mathbf{X}_j) (R_i + R_j - d_{i,j}) & \text{for } d_{i,j} \le R_i + R_j \end{cases}$$

The total repulsive forces exerted on the i-th particle by the other particles and the walls can be expressed as follows:

$$\mathbf{F}_i' = \sum_{j=1, j
eq i}^N \mathbf{F}_{i,j}^P + \mathbf{F}_i^W$$

'Fluidization/Sedimentation of many particles'



Efficient Data Structures

 $L3 \approx 220.000 \, elements \qquad \approx 1.100.000 \, d.o.f.s$

 $L4 \approx 880.000 \, elements \qquad \approx 4.400.000 \, d.o.f.s$

 $L5 \approx 3.530.000 \, elements \quad \approx 17.600.000 \, d.o.f.s$

 $\rm DEC/COMPAQ$ EV6, 833 MHz

CPU (s)			'brut	e force'		'improved'						
#PART		= 10		= 1000			= 10			= 1000		
items	L=3	L=4	L=5	L=3	L=4	L=5	L=3	L=4	L=5	L=3	L=4	L=5
NSE	17	88	440	16	80	403	17	95	423	17	83	435
Force	5	20	79	443	1771	7092	0	0	1	0	0	1
Particle	1	5	25	20	82	331	0	3	14	1	5	21
Total	24	114	546	480	1934	7827	18	98	439	18	89	468

Next: Efficient flow solver (for small Δt)???

Challenges



Adaptive time stepping + dynamical adaptive grid alignment/ALE





- (Better) collision models/Repulsive forces.
- Coupling with turbulence models.
- Modelling of Break-up/Coalescence phenomena.
- Deformable particles/fluid-structure interaction.
- Analysis of viscoelastic effects.
- Benchmarking and experimental validation for **many** particles.
- 1.000.000 particles.

Example for Deformed Meshes





Grid deformation preserves the (local) logical structure of the grid

Example for Deformed Meshes



Exact control and smooth transitions

Last Example

